USN

Sixth Semester B.E. Degree Examination, June/July 2014 Heat and Mass Transfer

Time: 3 hrs. Max. Marks: 100

Note: 1. Answer FIVE full questions, selecting at least TWO questions from each part.

2. Use of heat and mass transfer data handbook is permitted.

PART - A

- 1 a. What is thermal diffusivity? Explain its importance in heat conduction problems. (04 Marks)
 - b. Describe different types of boundary conditions applied to heat conduction problems.

(04 Marks)

- c. Consider a one dimensional steady state heat conduction in a plate with constant thermal conductivity in a region $0 \le x \le L$. A plate is exposed to uniform heat flux $q W/m^2$ at x = 0 and dissipates heat by convection at x = L with heat transfer coefficient h in the surrounding air at T_{∞} . Write the mathematical formulation of this problem for the determination of one dimensional steady state temperature distribution within the wall. (04 Marks)
- d. An industrial freezer is designed to operate with an internal air temperature of -20°C when the external air temperature is 25°C and the internal and external heat transfer coefficients are 12 W/m²°C and 8 W/m²°C, respectively. The wall of the freezer are composite construction, comprising of an inner layer of plastic 3 mm thick with thermal conductivity of 1 W/m°C. An outer layer of stainless steel of thickness 1 mm and thermal conductivity of 16W/m°C. Sandwiched between these layers is a layer of insulation material with thermal conductivity of 0.07 W/m°C. Find the width of the insulation required to reduce the convective heat loss to 15 W/m².
- 2 a. What is critical thickness of insulation on a small diameter wire or pipe? Explain its physical significance and derive an expression for the same. (10 Marks)
 - b. A set of aluminium fins (K = 180 W/mK) that are to be fitted to a small air compressor. The device dissipates 1 KW by convecting to the surrounding air which is at 20°C. Each fin is 100 mm long, 30 mm high and 5 mm thick. The tip of each fin may be assumed to be adiabatic and a heat transfer coefficient of 15 W/m²K acts over the remaining surfaces. Estimate the number of fins required to ensure the base temperature does not exceed 120°C. (10 Marks)
- 3 a. What are Biot and Fourier numbers? Explain their physical significance. (06 Marks)
 - b. What are Heisler charts? Explain their significance in solving transient convection problems.

 (06 Marks)
 - c. The temperature of a gas stream is measured with a thermocouple. The junction may be approximated as a sphere of diameter 1 mm, $K = 25 \text{ W/m}^{\circ}\text{C}$, $\rho = 8400 \text{ kg/m}^{3}$ and $C = 0.4 \text{ kJ/kg}^{\circ}\text{C}$. The heat transfer coefficient between the junction and the gas stream is $h = 560 \text{ W/m}^{2}\text{°C}$. How long will it take for the thermocouple to record 99% of the applied temperature difference?
- 4 a. Establish a relation between Nusselt, Prandtl and Grashof numbers using dimensional analysis. (08 Marks)
 - b. Explain velocity and thermal boundary layers. (06 Marks)

c. A 30 cm long glass plate is hung vertically in the air at 27°C while its temperature is maintained at 77°C. Calculate the boundary layer thickness at the trailing edge of the plate. Take properties of air at mean temperature $K = 28.15 \times 10^{-3}$ W/mK, $\gamma = 18.41 \times 10^{-6}$ m²/s, $P_r = 0.7$, $\beta = 3.07 \times 10^{-3}$ K⁻¹.

$\underline{PART - B}$

- 5 a. Explain the significance of: i) Reynolds number, ii) Prandtl number, iii) Nusselt number, iv) Stanton number. (08 Marks)
 - b. Atmospheric air at 275 K and free stream velocity 20 m/s flows over a flat plate of length 1.5 m long maintained at 325 K. Calculate:
 - i) The average heat transfer coefficient over the region where the boundary layer is laminar.
 - ii) Find the average heat transfer over the entire length 1.5 m of the plate.
 - iii) Calculate the total heat transfer rate from the plate to the air over the length of 1.5 m and width 1 m. assume transition occurs at a Reynolds number 2×10^5 . Take air Properties at mean temperature of 300 K.

 $K = 0.026 \text{ W/m}^{\circ}\text{C}, P_r = 0.708, \gamma = 16.8 \times 10^{-6} \text{ m}^2/\text{s}, \mu = 1.98 \times 10^{-5} \text{ kg/m-s}.$ (12 Marks)

- 6 a. Derive an expression for the effectiveness of a parallel flow heat exchanger. (10 Marks)
 - b. Engine oil is to be cooled from 80°C to 50°C by using a single pass counter flow, concentric-tube heat exchanger with cooling water available at 20°C. Water flows inside a tube with an internal dia of 2.5 cm with a flow rate of 0.08 kg/s and oil flows through the annulus at a rate of 0.16 kg/s. The heat transfer coefficient for the water side and oil side are respectively 1000 W/m²°C and 80 W/m²°C. The fouling factors are 0.00018 m²°C/W and 0.00018 m²°C/W, the tube wall resistance is negligible. Calculate the tube length required. Take specific heat of water as 4180 J/kg°C and for oil, 2090 J/kg°C. (10 Marks)
- 7 a. Explain film wise and drop wise condensation.

(04 Marks)

b. Draw the boiling curve and discuss the different regimes of boiling.

(08 Marks)

- c. Derive an expression for the total mass of water vapour diffused from a water column to the air passing over the water container. (08 Marks)
- 8 a. Explain briefly the concept of a black body.

(04 Marks)

b. State: (i) Kirchoff's law, ii) Plank's law, iii) Wien's displacement law.

(06 Marks)

c. Calculate the net radiant heat exchange per m² area for two large parallel plates at temperature of 427°C and 27°C respectively ∈ for hot plates is 0.9 and for cold plate it is 0.6. If polished aluminum shield is placed between them, find percentage reduction in the heat transfer. Assume ∈ for shield = 0.4. (10 Marks)

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